



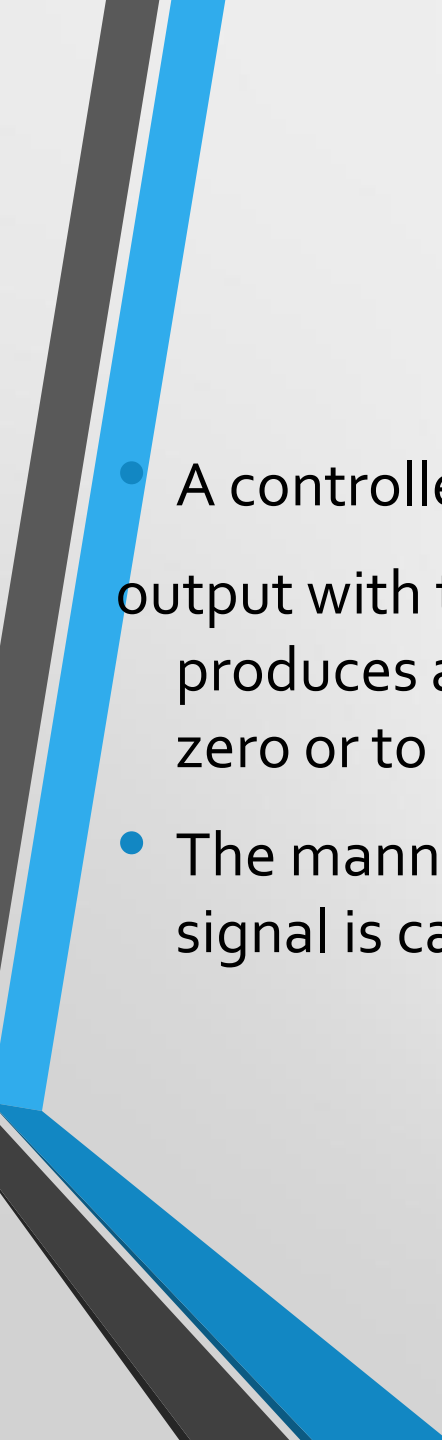
Control Systems



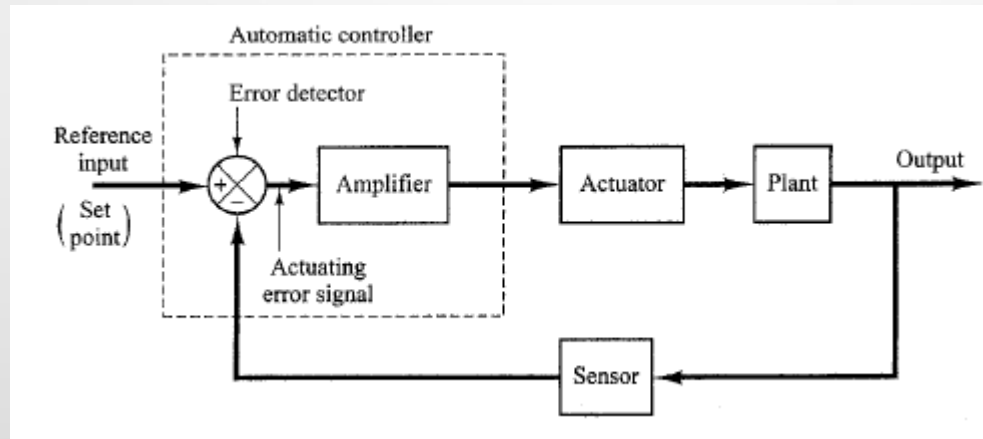
Lecture: 4

Topics Covered

- Basic Control Action
- P, PI, PID controller

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- A controller compares the actual value of output with the reference input, determines the deviation, and produces a control signal that will reduce the deviation to zero or to a small value.
 - The manner in which the controller produces the control signal is called the *control action*.

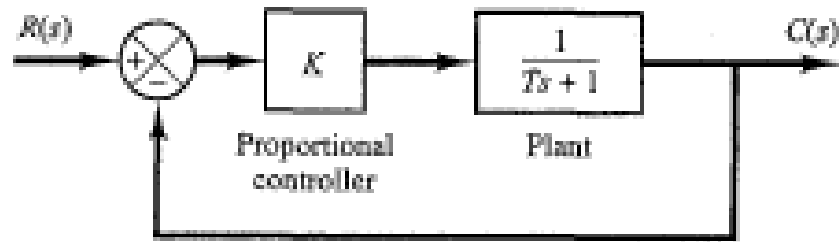
block diagram of an industrial control system



Classifications of Industrial Controllers.

- 1. Two-position or on-off controllers
- 2. Proportional controllers
- 3. Integral controllers
- 4. Proportional-plus-integral controllers
- 5. Proportional-plus-derivative controllers
- 6. *Proportional-plus-integral-plus-derivative controllers*

Pro



systems.

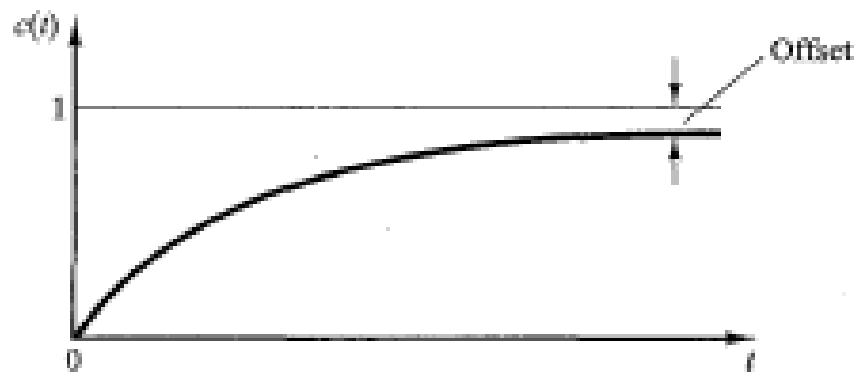
$$u(t) = K_p e(t)$$

$$\frac{U(s)}{E(s)} = K_p$$

$$\frac{E(s)}{R(s)} = \frac{R(s) - C(s)}{R(s)} = 1 - \frac{C(s)}{R(s)} = \frac{1}{1 + G(s)}$$

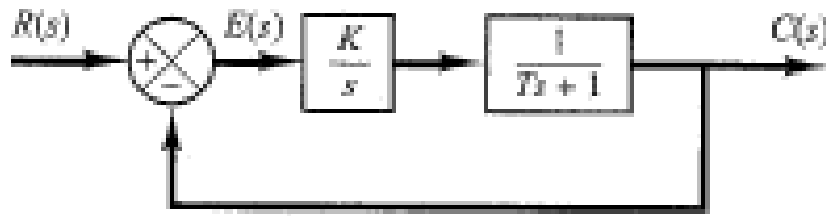
$$E(s) = \frac{Ts + 1}{Ts + 1 + K} \frac{1}{s}$$

$$e_{ss} = \lim_{t \rightarrow \infty} e(t) = \lim_{s \rightarrow 0} sE(s) = \lim_{s \rightarrow 0} \frac{Ts + 1}{Ts + 1 + K} = \frac{1}{K + 1}$$



error in the step
response is an offset.

Systems.



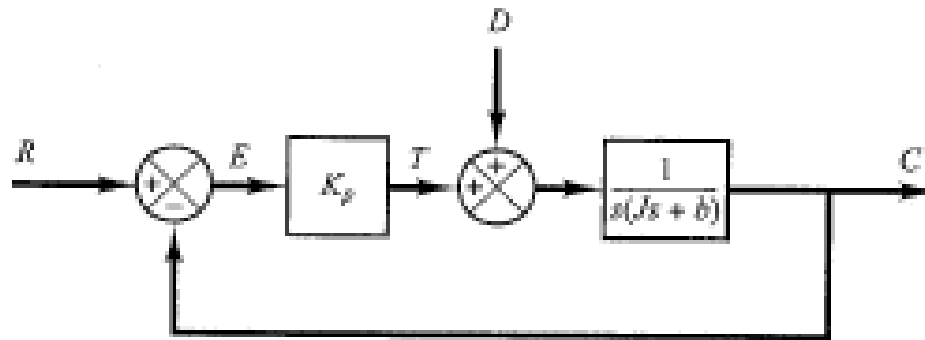
$$\begin{aligned} e_{ss} &= \lim_{s \rightarrow 0} sE(s) \\ &= \lim_{s \rightarrow 0} \frac{s^2(Ts + 1)}{Ts^2 + s + K} \frac{1}{s} \\ &= 0 \end{aligned}$$

Integral control of the system eliminates the steady-state error in the response to the step input..

Response to Torque Disturbances (Proportional Control)

Assuming that the reference input is zero or $R(s) = 0$, the transfer function between $C(s)$ and $D(s)$ is given by

$$\frac{C(s)}{D(s)} = \frac{1}{Js^2 + bs + K_p}$$



Hence

$$\frac{E(s)}{D(s)} = -\frac{C(s)}{D(s)} = -\frac{1}{Js^2 + bs + K_p}$$

The steady-state error due to a step disturbance torque of magnitude T_d is given by

$$\begin{aligned} e_{ss} &= \lim_{s \rightarrow 0} sE(s) \\ &= \lim_{s \rightarrow 0} \frac{-s}{Js^2 + bs + K_p} \frac{T_d}{s} \\ &= -\frac{T_d}{K_p} \end{aligned}$$

$$c_{ss} = -e_{ss} = \frac{T_d}{K_p}$$

Response to Torque Disturbances (Proportional-Plus-Integral Control)

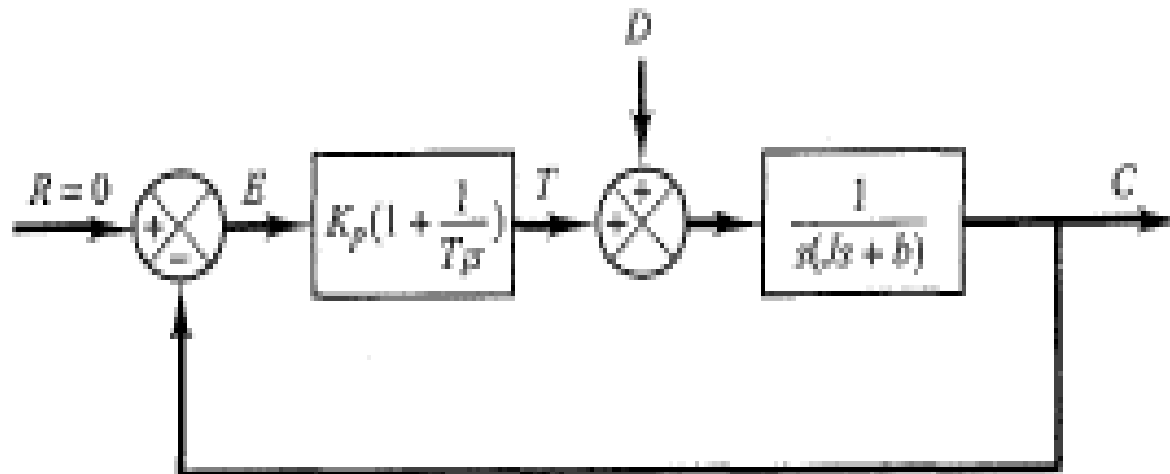
- To eliminate offset due to torque disturbance, the proportional controller may be replaced by a proportional-plus-integral controller.
- If integral control action is added to the controller, then, as long as there is an error signal, a torque is developed by the controller to reduce this error, provided the control system is a stable one.

The closed-loop transfer function between $C(s)$ and $D(s)$ is

$$\frac{C(s)}{D(s)} = \frac{s}{Js^3 + bs^2 + K_p s + \frac{K_p}{T_i}}$$

In the absence of the reference input, or $r(t) = 0$, the error signal is obtained from

$$E(s) = - \frac{s}{Js^3 + bs^2 + K_p s + \frac{K_p}{T_i}} D(s)$$



If this control system is stable, that is, if the roots of the characteristic equation

$$Js^3 + bs^2 + K_p s + \frac{K_p}{T_i} = 0$$

have negative real parts, then the steady-state error in the response to a unit-step disturbance torque can be obtained by applying the final-value theorem as follows:

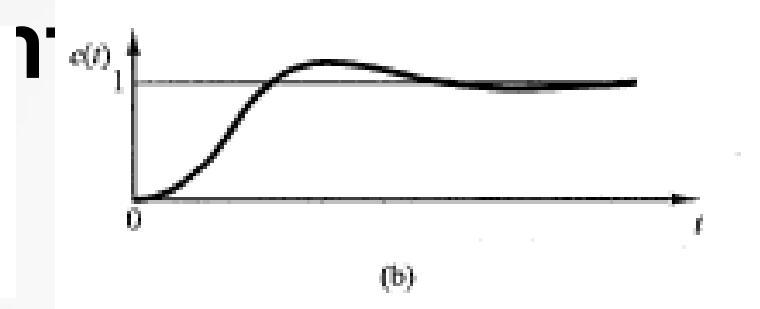
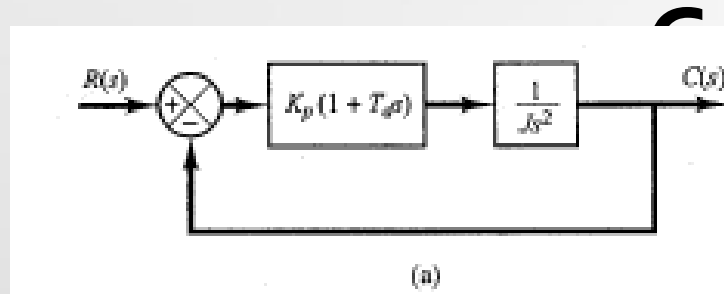
$$\begin{aligned} e_{ss} &= \lim_{s \rightarrow 0} sE(s) \\ &= \lim_{s \rightarrow 0} \frac{-s^2}{Js^3 + bs^2 + K_p s + \frac{K_p}{T_i}} \frac{1}{s} \\ &= 0 \end{aligned}$$

It is important to point out that if the controller was an integral controller, then the system always becomes unstable because the characteristic equation

$$Js^3 + bs^2 + K = 0$$

will have roots with positive real parts. Such an unstable system cannot be used in practice.

Proportional-Plus-Derivative



$$\frac{C(s)}{R(s)} = \frac{K_p(1 + T_d s)}{Js^2 + K_p T_d s + K_p}$$

. Thus derivative control introduces a damping effect. A typical response curve $c(t)$ to a **unit step** input is shown in

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- Effect of Proportional, Integral & Derivative Gains on the Dynamic Response

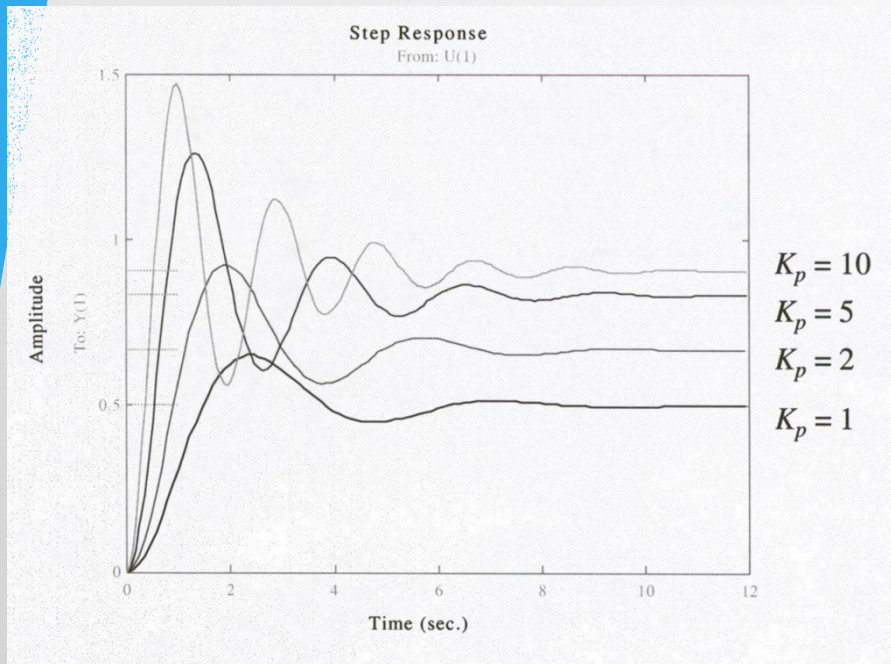
Change in gain in P controller

- Increase in gain:

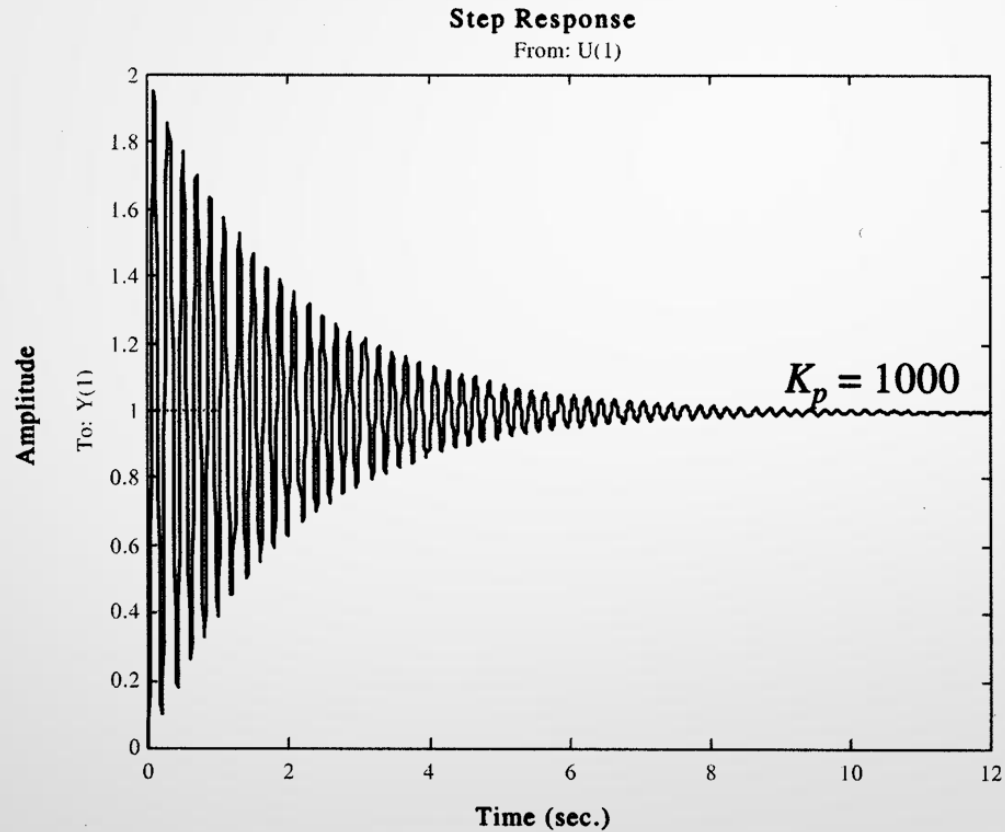
→ Upgrade both steady-state and transient responses

→ Reduce steady-state error

→ **Reduce stability!**



P Controller with *high* gain



Integral Controller

- Integral of error with a constant gain
 - increase the system type by 1
 - *eliminate steady-state error for a unit step input*
 - amplify overshoot and oscillations

Change in gain for PI controller

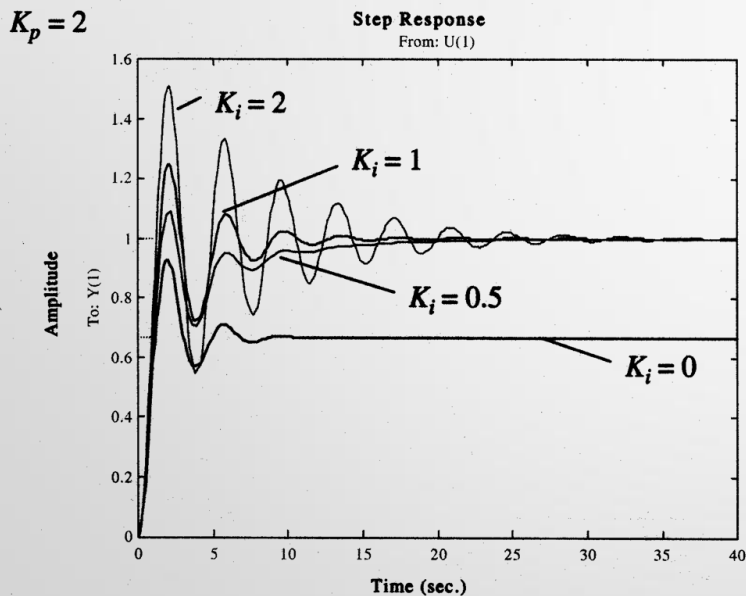
- Increase in gain:

→ Do not upgrade steady-

state responses

→ Increase slightly settling time

→ ***Increase oscillations and overshoot!***

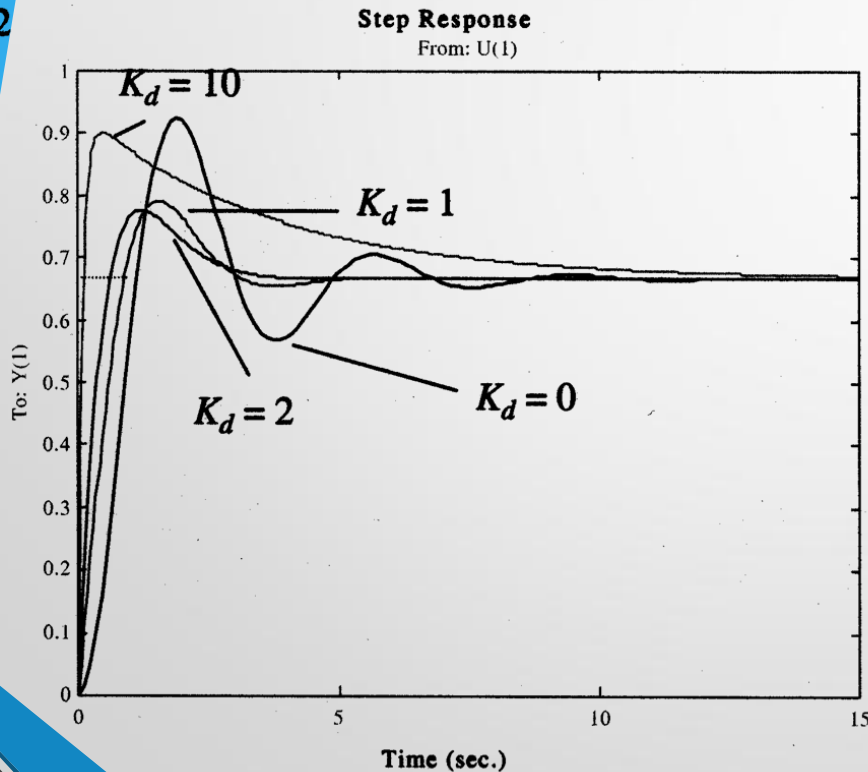


Derivative Controller

- Differentiation of error with a constant gain
 - detect rapid change in output
 - *reduce overshoot and oscillation*
 - do not affect the steady-state response

Effect of change for gain PD controller

$K_p = 2$



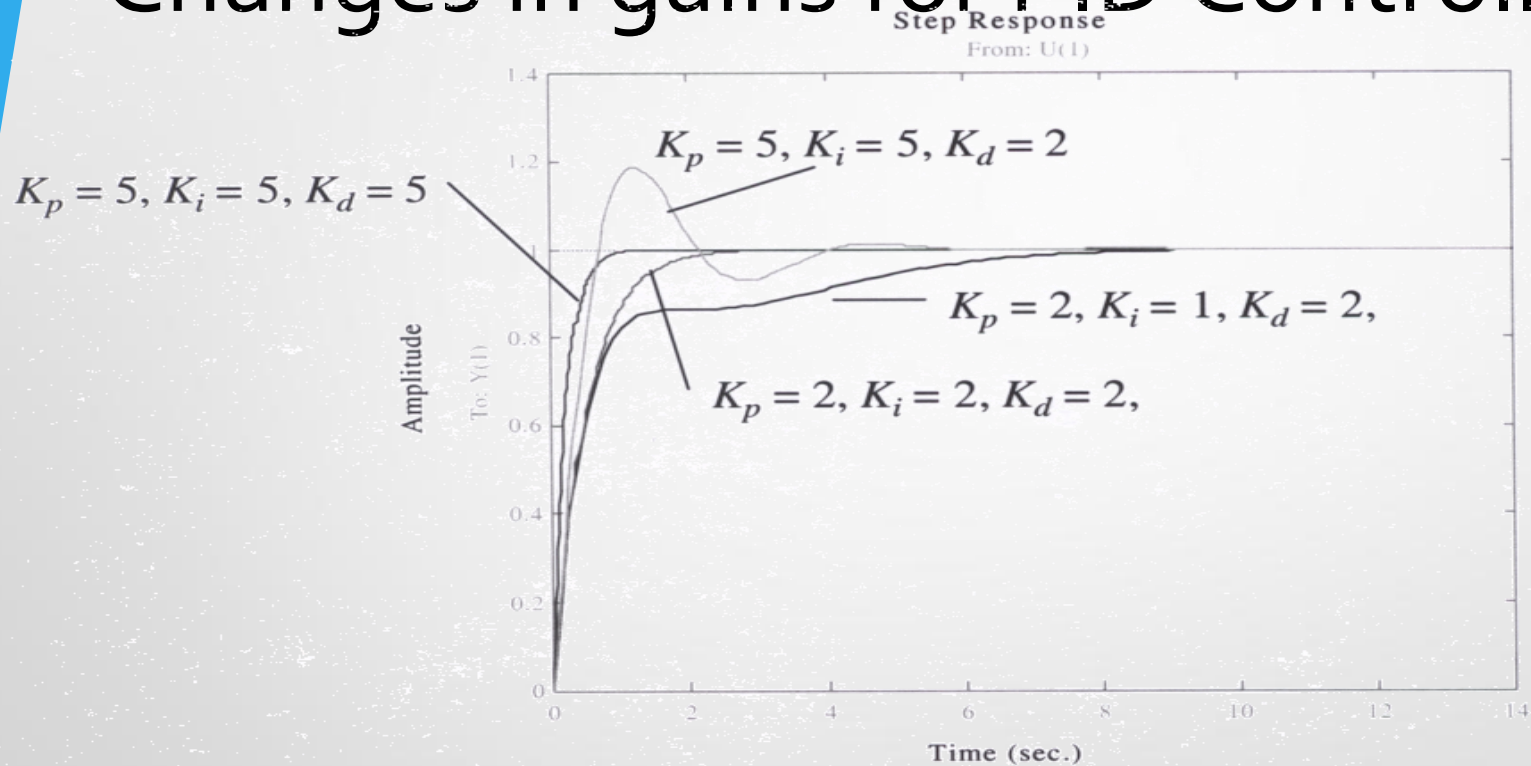
- Increase in gain:

→ Upgrade transient response

→ Decrease the peak and rise time

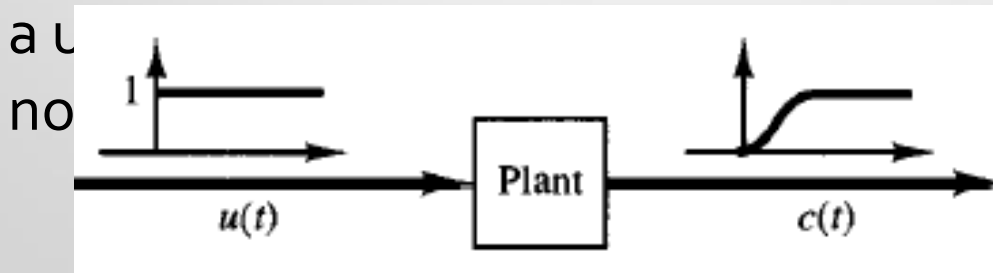
→ **Increase overshoot and settling time!**

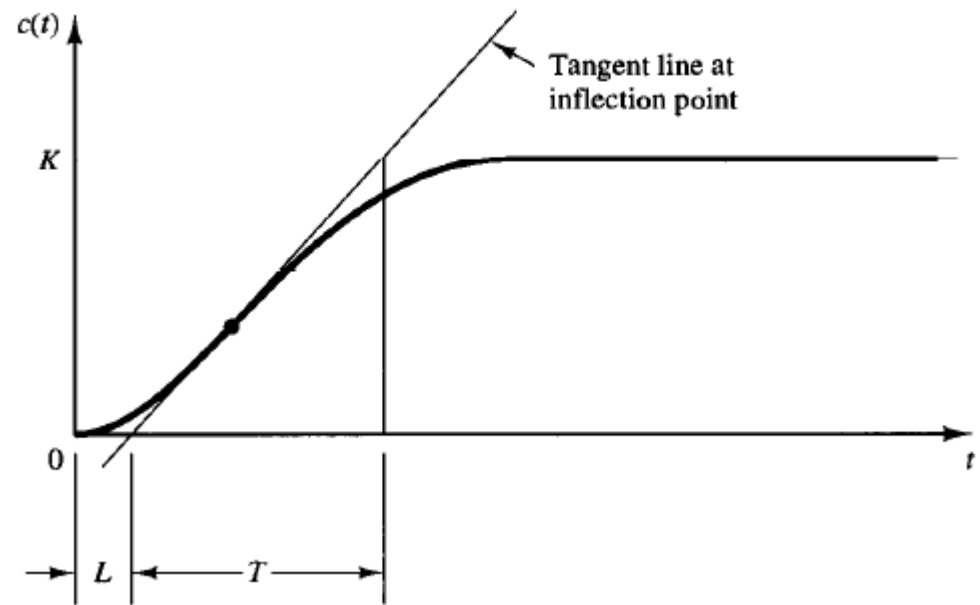
Changes in gains for PID Controller



Ziegler–Nichols rules for tuning PID controllers.

- These rules are used to determine K_p , T_i and T_d for PID controllers
- First Method: The response is obtained experimentally to a unit step input. The response is used to determine the parameters of the controller.





Ziegler and Nichols suggested to set the values of K_p , T_i , and T_d

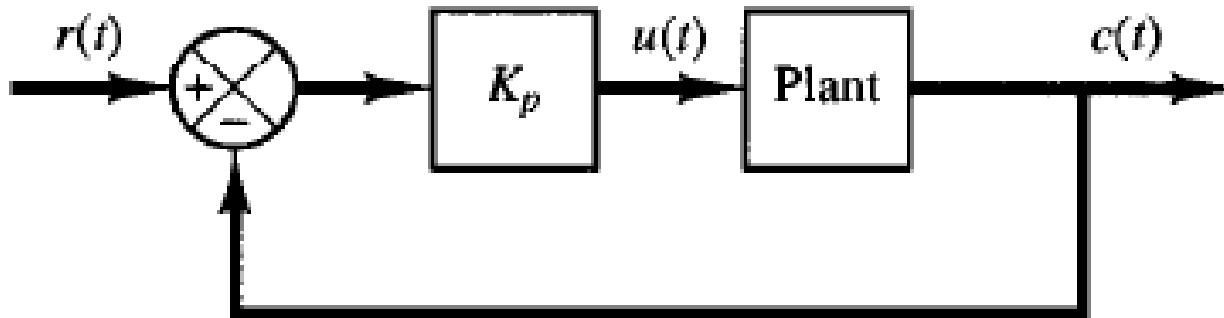
according to Table 10-1.

Table 10-1 Ziegler–Nichols Tuning Rule Based on Step Response of Plant (First Method)

Type of Controller	K_p	T_i	T_d
P	$\frac{T}{L}$	∞	0
PI	$0.9 \frac{T}{L}$	$\frac{L}{0.3}$	0
PID	$1.2 \frac{T}{L}$	$2L$	$0.5L$

Second Method

- Set $T_i = \infty$ and $T_d = 0$, increase K_p from 0 to a critical value K_{cr} where the output exhibits sustained oscillations.
- Use K_{cr} , T_{cr} and T_d to determine the parameters



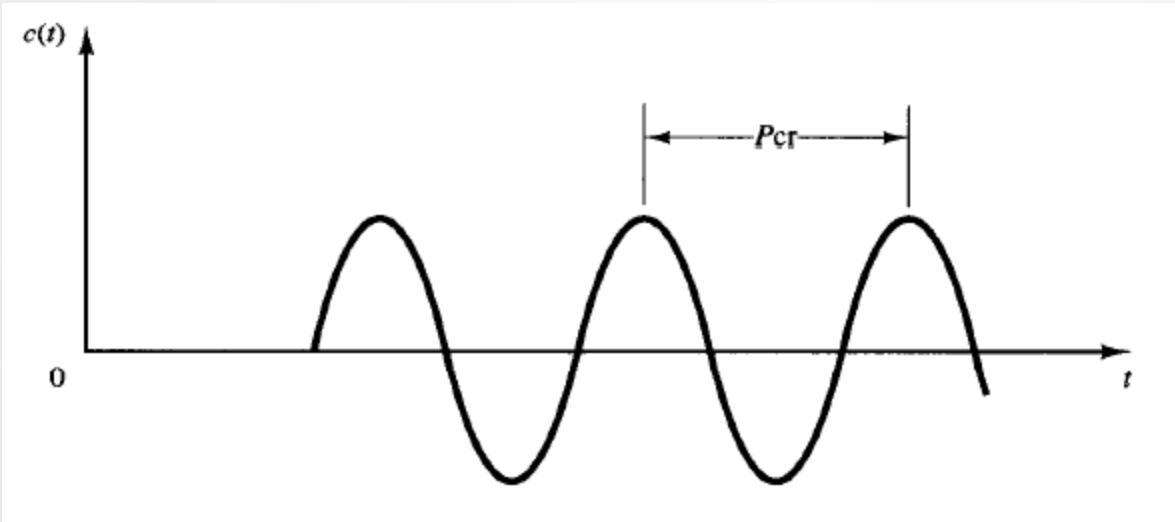


Table 10-2 Ziegler-Nichols Tuning Rule Based on Critical Gain K_{cr} and Critical Period P_{cr} (Second Method)

Type of Controller	K_p	T_i	T_d
P	$0.5K_{cr}$	∞	0
PI	$0.45K_{cr}$	$\frac{1}{1.2}P_{cr}$	0
PID	$0.6K_{cr}$	$0.5P_{cr}$	$0.125P_{cr}$